Phase 3 RFG: Preliminary Economic Impact Analysis and Related Issues

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Introduction

- Background
- Refinery Modeling Assumptions
- Preliminary Modeling Results
- Differences Compared To 1998 MTBE Study
- Factors Affecting Modeling Results
- Related Issues
- Closing Remarks

Background

- 1998 MTBE Study
- Executive Order D-5-99
- Phase 3 RFG Proposed Specifications
- Economic Analysis By CEC

Refinery Modeling Assumptions

- 1998 Properties
- Compliance Margins
- Emission Deltas
- Refinery Capacity
- Imports
- Exports
- Other Gasolines
- Cost Impacts

Assumptions - 1998 Properties

- CEC Survey October 1999
- Average In-Use Fuel Properties

—Rvp 6.78 psi

—Sulfur 21.8 ppm

—Benzene 0.59 vol. %

-Aromatics 23.42 vol. %

—Olefins 4.5 vol. %

-T50 200.8° F

-T90 309.7° F

Assumptions - Compliance Margins

- Flat Versus Average
- Difference Between Recipe And In-Use

—Rvp 0.22 psi

—Sulfur 4 ppm

—Benzene 0.18 vol. %

—Aromatics 1.9 vol. %

—Olefins 2.3 vol. %

-T50 4° F

-T90 7° F

Assumptions - Emission Deltas

- Predictive Model
- Candidate Versus Reference Fuels
- Deltas For NO_x, THC, And Toxics
- Deltas Not Zero For Each Pollutant
- Refinery Modeling Deltas
 - $-NO_x$ target of -0.2
 - —THC target of -0.1
 - —Toxics target of -0.2

Assumptions - Refinery Capacity

- Capacity Creep By 2003
- Low Sulfur Levels For Specific Components
 - —Alkylate at 2 ppm
 - —Hydrocrackate & reformate at 1 ppm
- Additional Capacity Build For Each Case Possible Refinery Modeling Outcome
- Additional Imports Possible Refinery Modeling Outcome

Assumptions - Imports

- Model Can Import Ethanol & Various Gasoline Blending Components
- Supply Cost Curves
- Values Compared To 1998 Study
 - —CARBOB increased by 2 cents per gallon
 - —Alkylate increased by 7 cents per gallon
 - —Ethanol increased by 27 to 48 cents per gallon
- Alkylate Quality C7, Not Mixed
- Alkylate Limited To 111 TBPD

Assumptions - Exports

- Some Components Not Suitable For Use Under Various Cases
 - —Pentanes
 - —Light FCC Gasoline
- Products Exported To Markets Outside State At Low Values

Assumptions - Other Gasolines

- California Refineries Also Produce Gasoline For Arizona And Nevada
- 2003 AZ Gasoline Will Use Ethanol
- 2003 Nevada Gasoline Will Not Contain Any Oxygenates
- Gasoline Qualities Assumed Not To Become Poorer Through Dumping

Assumptions - Cost Impacts

- Change In Production Cost Compared To Base Case
- Average Cost Impact Calculation
 - —Variable Costs
 - —Refinery Capital Charges
 - —Ancillary Refining Costs
 - —Logistics Costs
 - -Mileage Change Impact

Preliminary Modeling Results

- Base Cases
 - —Predictive model change
- Ethanol At 2.0 Wt. Percent
 - —MTBE phaseout impact
 - —Phase 3 RFG specifications impact
 - Less stringent distillation temperature impact
 - —Less stringent volatility impact

Results - Base Case

- MTBE In Use
- Phase 3 Predictive Model
- Average Cost Declines 0.2 Cents Per Gallon

Results - Case 1A, No MTBE

- No MTBE, Ethanol At 2.0 Wt. %
- Phase 3 Predictive Model
- Average Cost Increases 5.5 Cents Per Gallon
- Refinery Investment \$348 Million
- 111 TBPD Imported Alkylate
- 47 TBPD Rejected Blendstocks
- Expensive Imports Primary Factor

Results - Case 2A, ARB Proposal

- No MTBE, Ethanol At 2.0 Wt. %
- Phase 3 Predictive Model
- Average Cost Increases 6.4 Cents Per Gallon
- Refinery Investment \$564 Million
- 111 TBPD Imported Alkylate
- 49 TBPD Rejected Blendstocks
- Expensive Imports Primary Factor
- Additional Refinery Modifications

Results - Case 3A, Higher Distillation Temperatures

- No MTBE, Ethanol At 2.0 Wt. %
- Phase 3 Predictive Model
- Average Cost Increases 5.2 Cents Per Gallon
- Refinery Investment \$411 Million
- 111 TBPD Imported Alkylate
- 39 TBPD Rejected Blendstocks
- Expensive Imports Primary Factor

Results - Case 4A, Higher Volatility (Rvp)

- No MTBE, Ethanol At 2.0 Wt. %
- Phase 3 Predictive Model
- Average Cost Increases 5.7 Cents Per Gallon
- Refinery Investment \$442 Million
- 111 TBPD Imported Alkylate
- 49 TBPD Rejected Blendstocks
- Expensive Imports Primary Factor

Results - Comparing Current Cases

- Using Phase 3 Predictive Model Decreases Average Costs 0.2 Cents
- Phasing Out MTBE Increases Average Costs 5.7 Cents Per Gallon
- Phase 3 RFG Specifications Increase Average Costs 0.9 Cents Per Gallon

Results - Comparing Current Cases (cont.)

- Higher Distillation Temperatures Decrease Average Costs 1.2 Cents Per Gallon
- Increasing Rvp 0.1 PSI Decreases Average Costs 0.7 Cents, Compared To Current ARB Proposal

Differences Compared To 1998 MTBE Study

- Similar 1998 Ethanol Case Resulted In Average Cost of 1.9 cents Per Gallon Versus 6.4 Cents Today
- Primary Reasons:
 - —Higher cost of ethanol
 - —Higher cost of alkylate
 - —Different fuel specifications

Factors Affecting Modeling Results

- Could Average Cost Impacts Decrease?
- Could Average Cost Impacts Increase?

Factors Which Could Decrease Average Cost

- Less Expensive Ethanol
 - —Over build of ethanol supply
 - —Elimination of federal oxygen requirement
 - —Elimination of import tariff
- Less Expensive Alkylate
 - —Over build of alkylate supply
 - Production of iso-octane from converted
 MTBE facilities

Factors Which Could Decrease Average Cost (cont.)

- Decreased Marine Shipping Costs
 - —Elimination of Jones Act
- Ability To Ship Ethanol Blends Through Pipeline Distribution Infrastructure
- Increase In Availability Of Desirable Blending Components
 - —Lower sulfur standards in rest of U.S.

Factors Which Could Increase Average Cost

- More Expensive Ethanol
 - —Under build of ethanol supply
 - -MTBE ban outside California
 - —Elimination of federal excise tax credit
- More Expensive Alkylate
 - —Under build of alkylate supply
 - —Greater demand for alkylate
 - -MTBE ban outside California

Factors Which Could Increase Average Cost (cont.)

- Decrease In Ability Of Importers To Continue Supplying California
 - —No investments to meet new fuel specifications
- Decrease In Availability Of Desirable Blending Components
 - —Cleaner components being used to meet stricter fuel standards in U.S. and Europe
 - No alkylate available, refiners build sufficient capacity

Related Issues

- Lower Sulfur Modeling Runs
- Refinery Capacity
- Price Volatility

Related Issues - Lower Sulfur Standards

- Modeling Runs For Sulfur Limit Of 2 PPM and Cap Of 5 PPM Not Run
 - Expense of lowering average to 5 PPM in PADDs 1 - 3 Estimated At 2 to 3 Cents
 - —Achieving the SC5 standard appears technically feasible, but only with advanced new desulfurization technologies and significant changes in refinery operation.
 - —Technology to produce gasoline at average of 2 not currently available

Related Issues - Lower Sulfur Standards

- Additional Expense Of Lowering
 Average Sulfur Content To 2 PPM Is
 Expected To Be Much Greater Than 3
 Cents Per Gallon
 - Additional cost of phase 3 RFG proposal only 0.9 cents per gallon
- Cap Of 5 PPM Could Limit Ability Of Refiners To Consistently Produce Complying Gasoline

Related Issues - Refinery Capacity

- Aggregate Refinery Modeling Results May Not Be Indicative Of Individual Company Investment Decisions
 - Refinery production capacity could decline if refiners choose not to make up for all of the lost volume
 - —CEC initial estimate of 5 to 10 percent decline
 - —ARB initial estimate of 10 to 20 percent decline

Related Issues - Price Volatility

- Phase Out Of MTBE And More Stringent Fuel Specifications Could Result In Greater Price Volatility For California
- Today s Minor Unplanned Outages Will Have Greater Impact In The Future
 - Future outages will degrade ability to make same volume of complying gasoline

Closing Remarks

- Additional Modeling Runs Prior To December 9 Board Hearing
 - —Ethanol at different volumes
 - —No oxygenates
 - —Combination of ethanol and no oxygenates